

Sol–gel derived silver doped nanocrystalline titania catalysed photodegradation of methylene blue from aqueous solution

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Abstract

Nanocrystalline pure anatase titania doped with silver was prepared by sol–gel process at room temperature followed by ultrasonication (Ti–Ag–US). The photocatalytic activity of Ti–Ag–US has been evaluated by the degradation of textile dye, methylene blue in presence and absence of common inorganic salts (nitrate, acetate and sulphate). It was observed that in presence of anions the degradation of the dye increases significantly. The influence of the presence of H_2O_2 on the degradation rate was studied. The dependence of photodegradation of the dye rates on various parameters such as dye concentration, photocatalyst concentration and pH were also investigated. The photodegradation rate follows pseudo first order kinetics. H_2O_2 and UV light have a negligible effect in absence of Ti–Ag–US catalyst. The relative photonic efficiency of the system is reported using phenol as a standard organic compound.

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1. Introduction

Dye pollutants from the textile industry are an important source of environmental contamination. It is estimated that from 1 to 15% of the dye is lost during dyeing processes and is released in waste waters [1]. The release of these colored waste waters in the eco system is a dramatic source of aesthetic pollution, eutrophication and perturbations in aquatic life [2].

A variety of physical, chemical and biological methods are presently available for treatment of textile waste water. Biological treatment is a proven technology and is cost effective. However, it has been reported that the majority of dyes are only adsorbed on the sludge and are not degraded [3]. Physical methods such as ion-exchange, adsorption, air stripping, etc., are also

ineffective on pollutants which are not readily adsorbable or volatile, and have the further disadvantage that they simply transfer the pollutants to another phase rather than destroying them. This leads to search for highly effective method to degrade the dyes into environmentally compatible products. It has been revealed from the literature that photocatalysis can be used to destroy the dyes using semiconductor catalyst under light irradiation [4,5]. Among the semiconductors used, TiO_2 is considered particularly efficient owing to the formation of electron–hole pair under illumination with near UV light. The activity of titania is influenced by several factors such as crystallinity of the anatase phase [6,7], particle size, surface area [8,9] and the method of preparation [10,11]. It is known that the transformation from amorphous to anatase or rutile phase is influenced by the preparative experimental conditions [12]. Different preparation methods such as hydrolysis, sol–gel, microemulsion or reverse miscelles, hydrothermal and mechano chemical method [13] are

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reported by several researchers [14–19] to synthesize nanoparticles of titania. The ultrasonication technique is extensively used for the preparation of mesoporous titania [20], anatase and rutile titania [21] and brookite titania [22], titania nanotubes [23] ZnO nano crystals [24], MCM-41 silica [25]. Several metals were used for doping especially Pt^0 , Li^+ , Zn^{2+} , Cd^{2+} , Mn^{2+} , Ce^{3+} , Cr^{3+} , Fe^{3+} and Al^{3+} . Platinization of titania has been proposed in early 1978 for the photocatalytic transformation of acetic acid [26]. The presence of transition metals may increase the photocatalytic activity by scavenging electrons that render the recombination of charges and favour the formation of hydroxyl radical. High concentration of metal (Cu^{2+} , Ni^{2+}) may have the detrimental effect either by competitive trapping of oxidizing species h^+ and OH^\bullet or by filter effect when salts significantly absorbed in UV range. Besides the redox potentials of Cu/Cu^+ , $\text{Cu}^+/\text{Cu}^{2+}$ and $\text{Fe}^{2+}/\text{Fe}^{3+}$ permit the formation of photocurrent. With Pt and Pd salts deposition of Pt^0 and Pd^0 may occur on the particles of TiO_2 [27]. Okamoto et al. [28] reported that the influence of Ce^{2+} may be positive or negative according to the concentration. Kiriakidodu et al. [29] reported that the addition of Ca^{2+} to titanium significantly decreases the photocatalytic decomposition of acid orange 7, whereas the presence of W^{6+} has a significant positive effect for the small per cent of W^{6+} . It is believed that different processes may be involved according to experimental conditions hence it is difficult to assess the influence of transition metal on photocatalysis and experiments are necessary to point out the effect of these metals.

In this present work, we report on the novelty of ultrasonication technique coupled with sol–gel method for the synthesis of nanocrystalline single phase pure anatase titania doped with silver (Ti–Ag–US) at room temperature while others have reported mixed phases [15,21]. The influence of this irradiated photocatalyst on the degradation of MB in aqueous system was reported. Its structure is presented in Fig. 1. The parameters studied include irradiation time, effect of initial MB concentration, concentration of nanocrystalline Ti–Ag–US, effect of H_2O_2 , effect of common inorganic salts and pH.

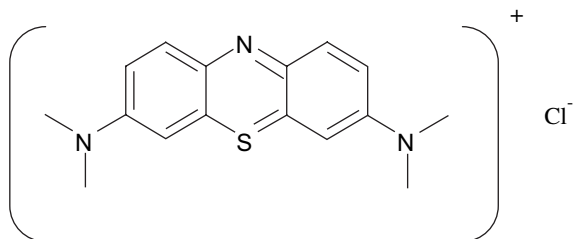


Fig. 1. Structure of methylene blue.

2. Materials and methods

2.1. Chemicals

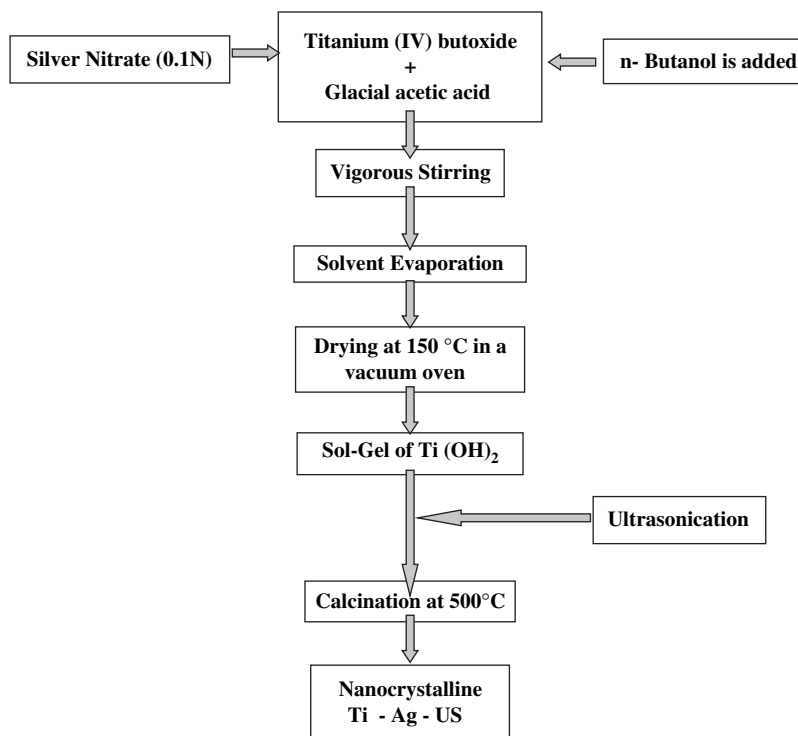
Titanium (IV) *n*-butoxide (99%) was purchased from Lancaster and used as such. Analar grade glacial acetic acid and *n*-butanol were obtained from SD's Fine Chemicals and were triply distilled. The analar quality sodium salt of NO_3^- , SO_4^{2-} , acetate, H_2O_2 (100 volumes), Silver nitrate and dye methylene blue (MB) were procured from SD's Fine Chemicals and used as received.

2.2. Synthesis of nanocrystalline TiO_2

The experimental flow chart for the synthesis of TiO_2 bulk is given in Fig. 2. Detailed procedure for the preparation of TiO_2 is discussed as follows: titanium (IV) *n*-butoxide (3.5 g) is added to 4 g of glacial acetic acid with constant stirring. To the reaction mixture, *n*-butanol (42.5 g) and silver nitrate (0.1 N) are added slowly. The total volume of the reactants is maintained to be 100 ml. The contents are stirred vigorously for 6–8 h. The excess solvent is evaporated by drying in a vacuum air oven at 150 °C for 12 h. The TiO_2 sol obtained was ultrasonically treated for 30 min. The derived gel is subjected to calcination at 500 °C for 30 min and labeled Ti–Ag–US. The final product is ground to get fine particles. In case of titanium alkoxide precursors, dilute solutions of the reactants, i.e., water (hydroxyl group precursor) and alkoxide (titanium precursor) in excess ethanol allow physical separation of the reactants. But titanium butoxide is extremely water sensitive precursor. Therefore, the maximum titania loading that can be achieved without second phase precipitation of titania is limited. In general, as the loading of the dispersed phase is increased we can see the precipitation of a second phase [30]. The XRD pattern of Ti–Ag–US was recorded on Shimadzu X-Ray diffractometer over a 2θ range of 20–80° with a step size of 0.02° and a collection time of 0.3 s ($\lambda = 1.541$). The strongest peak at $2\theta = 25.2^\circ$ is representative for (101) anatase phase reflections, where by applying the Scherrer's formula, the Ti–Ag–US crystallites size can be estimated at 44 nm [31].

2.3. Photocatalytic decomposition of methylene blue

Experiments were performed in an open thermostated pyrex reactor of 250 ml capacity and provided with water circulation arrangement in order to maintain the temperature. The suspensions in the reactor were left for 60 min in dark in order to achieve the maximum adsorption of the dye on to Ti–Ag–US surface. The irradiation was carried out using 125 W (311 nm) medium pressure Hg arc lamp. The average light

Fig. 2. Synthesis of nanocrystalline $\text{TiO}_2\text{-Ag}$.

intensity on the reaction vessel at a distance of 15 cm from the lamp was found to be 1.6×10^{-4} Einstein min^{-1} .

In all the studies, 150 ml of MB solution containing an appropriate amount of Ti-Ag-US was magnetically stirred, before and during illumination. At specific time intervals, 5 ml of the sample was withdrawn and filtered through $0.45 \mu\text{m}$ filters. Changes in the concentration of MB were observed from its characteristic absorption at 666 nm using a UV-vis spectrophotometer (Schimadzu UV-1601). The influences of (0.025 M) anions such as nitrate, sulphate and acetate on the photodegradation of MB (10 mg/L) in presence of Ti-Ag-US (330 mg/L) at pH (6.80) were studied. All experiments, except were otherwise mentioned in the text, were carried out at natural pH (6.80).

3. Results and discussion

3.1. Adsorption isotherm

Adsorption tests in dark conditions were carried out in order to evaluate the equilibrium constants of the adsorption of dye on the TiO_2 surface at different concentrations. The extent of equilibrium adsorption was determined from the decrease in dye concentration. The amount of dye molecules adsorbed on Ti-Ag-US was determined by Eq. (1) [32],

$$n = \frac{V\Delta C}{W} \quad (1)$$

where n is the number of dye molecules adsorbed per gram of Ti-Ag-US , ΔC the decrease in the dye concentration in mg/L, W the weight of Ti-Ag-US in grams and V is the volume of dye solution in litre. The value of n_{max} for the equilibrium of adsorption of MB was calculated as 5.61 mg/g from the following Eq. (2),

$$\frac{C_{\text{eq}}}{n} = \frac{1}{Kn_{\text{max}}} + \frac{C_{\text{eq}}}{n_{\text{max}}} \quad (2)$$

where n is the number of adsorption sites on Ti-Ag-US , C_{eq} is the equilibrium concentration of dye and K is the equilibrium constant for MB adsorption.

3.2. Change of absorption spectra

Fig. 3 shows the change in absorption spectrum of 10 ppm MB on irradiation in an aqueous solution containing 0.125 mg/L Ti-Ag-US . The absorption spectrum is seen to decrease in intensity with increase in irradiation time. The rapid decrease in the intensity of 666 nm band in Fig. 3 suggests that the chromophore responsible for characteristic color of the MB is breaking down.

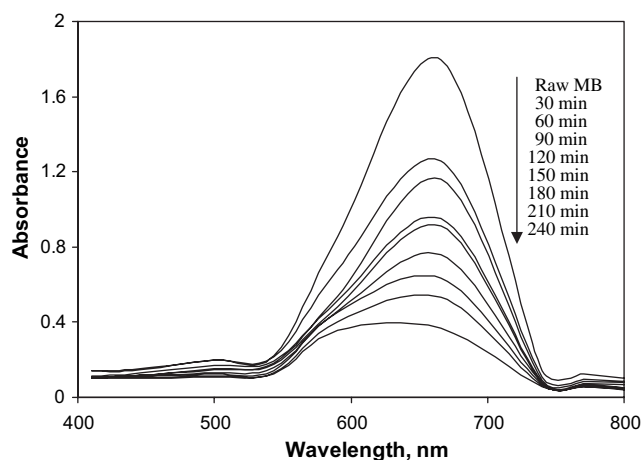


Fig. 3. Change of absorption spectra of MB with irradiation time.

3.3. Effect of initial MB concentration and irradiation time

Fig. 4 shows the normalized concentration vs. irradiation time for different initial MB concentrations at fixed Ti–Ag–US concentration. The experimental kinetic data follow the pseudo first order kinetic expression, which is rationalized in terms of the Langmuir–Hinshelwood model modified to accommodate reactions occurring at a solid–liquid interface [33,34].

$$r_0 = -\frac{dc}{dt} = \frac{k_r K C_{eq}}{1 + K C_{eq}} \quad (3)$$

where r_0 is the initial rate of disappearance of the organic substrate and C_{eq} is the equilibrium bulk solute concentration. K represents the equilibrium constant for adsorption of the organic substrate onto Ti–Ag–US and k_r reflects the limiting rate of reaction at maximum coverage under the given experimental conditions. This equation can be used when the data demonstrate linearity when plotted as follows:

$$\frac{C_{eq}}{r_0} = \frac{1}{k_r K} + \frac{C_{eq}}{k_r} \quad (4)$$

The photodecomposition of various initial concentrations of MB in the presence of fixed amount of Ti–Ag–US is illustrated in Fig. 4, which depicts the distinction equilibrium between the dark adsorption–desorption equilibrium and the additional decrease in MB concentration caused by UV illumination. From Fig. 4 it is clear that MB is adsorbed strongly on Ti–Ag–US. For this reason, the equilibrium concentration of the CV dye (C_{eq}), instead of the initial one, has been used in the kinetic study [35,36]. The k_r and K values

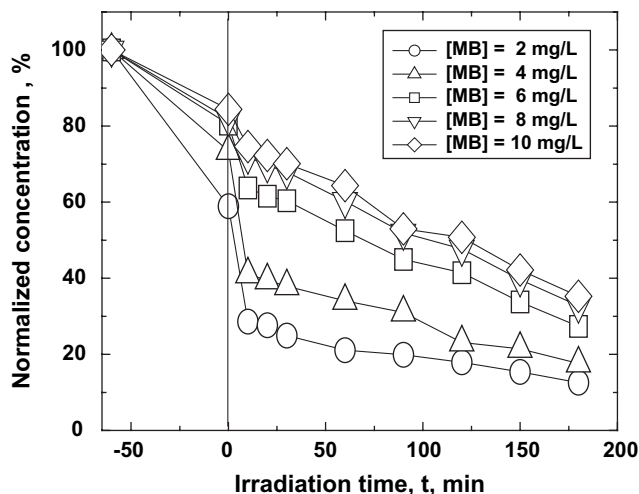


Fig. 4. Effect of initial concentration and irradiation time on MB degradation. Conditions: [Ti–Ag–US] = 333 mg/L; pH = 6.80.

were calculated from the slope and the intercept of C_{eq}/r_0 vs. C_{eq} plot (Fig. 5) and found to be 0.0199 mg/L min and 0.3689 L/mg, respectively.

3.4. Effect of catalyst concentration

Experiments were carried out with different concentrations of catalyst (0.200–0.533 g/L) at fixed MB concentration (10 mg/L). It has been observed that the initial rate increases with an increase in the amount of catalyst and that it remains almost constant above a certain level and is presented in Table 1. This has been explained as the concentration of the catalyst is increased; the number of photons absorbed and the number of dye molecules adsorbed are increased with respect to an increase in the number of catalyst

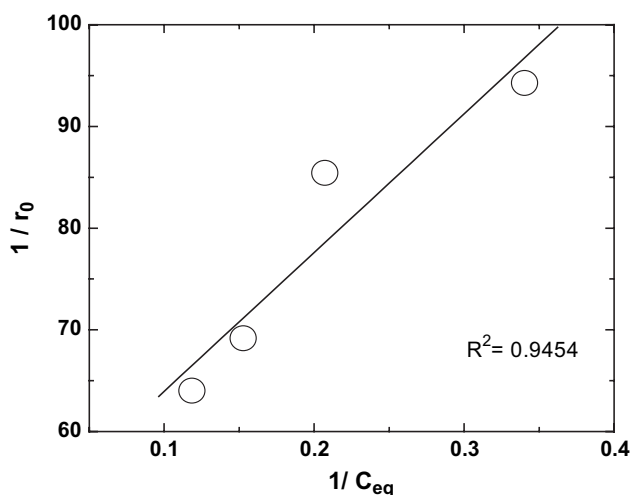
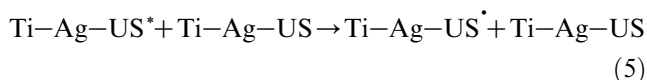


Fig. 5. Kinetics of photocatalytic MB degradation. Conditions: [Ti–Ag–US] = 333 mg/L; pH = 6.80.

Table 1
Effect of Ti–US concentration on the decolorization rate

[TiO ₂] (g/L)	<i>r</i> ₀ (mg/L min)
0.200	0.0517
0.267	0.0630
0.333	0.0920
0.400	0.2193
0.533	0.3147

molecules. The density of the molecule in the area of illumination also increases and thus the rate gets enhanced. After a certain level, the dye molecules available are not sufficient for adsorption by the increased number of catalyst molecule. Hence, the additional catalyst powder is not involved in the photocatalytic activity and the rate does not increase with increase in the amount of catalyst beyond certain limit. It is also expected that the aggregation of the catalyst molecules at high concentration must also be considered, which causes the decrease in the number of active surface sites. The experimental data are found in good agreement with those reported by Sauer et al. [37] for the degradation of Safira dye using Degussa P-25. Neppolian et al. [38] also reported the decreased per cent degradation of reactive dyes at higher catalyst concentration. Further, it is explained that the deactivation of activated molecule by collision with the ground state molecule with the shielding of TiO₂ may also take place according to Eq. (5),



where Ti–Ag–US* is the Ti–Ag–US with active species adsorbed in its surface and Ti–Ag–US[·] the deactivated form of Ti–Ag–US. Hence, an optimum catalyst concentration has to be maintained to ensure total absorption of photons for efficient photodegradation [39].

Galindo et al. [1] reported an empirical initial degradation rate and catalyst concentration as $r_0 \propto [\text{TiO}_2]^n [\text{dye}]$ where *n* is the exponent less than one for the dye studied in reaction to the lower concentration of catalyst. In our present work, the initial degradation rate follows a similar relationship and the ‘*n*’ value was found to be 2.05 when the Ti–Ag–US concentration was less than 1.0 g/L (Fig. 6).

3.5. Effect of pH

The influence of pH on the decolorization of MB is shown in Fig. 7. The results showed that there was a strong dependence of pH of the solution on the heterogeneous photoprocess. It is known that the metal oxide particles suspended in water behave similar to

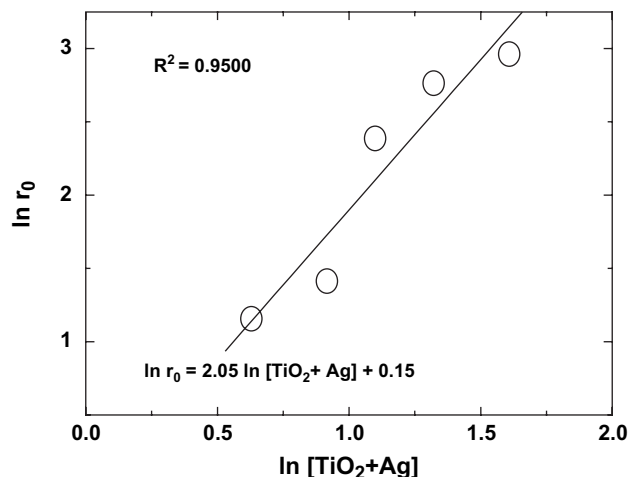


Fig. 6. Effect of catalyst concentration on MB degradation rate. Conditions: [MB] = 10 mg/L; pH = 6.80.

diprotic acids. For TiO₂, hydroxyl groups undergo two acid base equilibria:



Generally, for charged substrates, a significant dependency of the photocatalytic degradation efficiency on pH value had been observed, since the overall surface charge and hence the adsorptive properties of TiO₂ particles depend strongly on solution pH [40,41].

In our experiments, any changes in initial degradation rate with varying pH values must be ascribed to variations of the acid/base properties of the Ti–Ag–US particle surface (Eqs. (6) and (7)). Since the photooxidation of dyes is accompanied by the release of protons

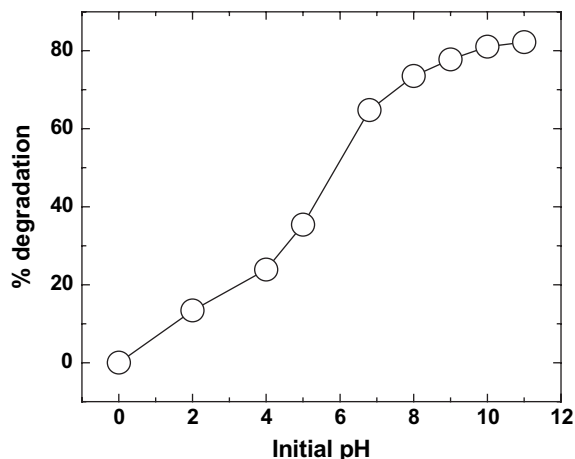


Fig. 7. Effect of initial pH on MB degradation. Conditions: [MB] = 10 mg/L; [Ti–Ag–US] = 333 mg/L; irradiation time = 3 h.

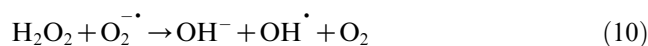
[42], its efficiency may then change because of the reversible protonation of the Ti–Ag–US surface. The MB is a cationic dye in aqueous solution. In acidic pH range ($\text{pH} < 6.8$), Ti–Ag–US acquires positive charge and hence electrostatic repulsion between Ti–Ag–US and dye cation retards the degradation rate. On the other hand, in basic pH ($\text{pH} > 6.8$), electrostatic interaction between the negative Ti–Ag–US and dye cation leads to strong adsorption with the corresponding high rate of degradation and reaches a maximum at pH 10. This behaviour is characteristics for many photocatalytic systems and similar results have been reported by the photodegradation of other dyes [42].

3.6. Effect of H_2O_2 on the photodegradation of MB

Experiments were conducted to evaluate the effect of H_2O_2 on the MB photodegradation (Fig. 8). In our study, photocatalytic efficiency increases as the concentration of H_2O_2 increases and reaches optimum at 3.4 mg/L and further increases in concentration up to 6.8 mg/L leading to decrease in the photodegradation rate. The addition of H_2O_2 increases the concentration of OH^\bullet radical since it inhibits the e^- , h^+ recombination according to the Eq. (8),



H_2O_2 is considered to have two functions in the photocatalytic degradation. It accepts a photogenerated conduction band electron thus promotes the charge separation (Eq. (9)) and it also forms OH^\bullet (Eq. (10)).



The addition of H_2O_2 is a well known mechanism to increase the rate of photocatalytic degradation with higher quantum yield of formation of OH^\bullet [43,44]. Consequently, the degradation rate is expected to be increased. Further increase of H_2O_2 after the quantum level, decreases the rate of degradation slowly. This negative effect of high concentration of H_2O_2 may be due to the formation of OH_2^\bullet . When the H_2O_2 concentration is higher, OH_2^\bullet formed is significantly less reactive than OH^\bullet . Wang and Hong [45] reported that the H_2O_2 on the catalyst surface acts as a powerful OH^\bullet scavenger (Eqs. (11) and (12)) along with a photo-generated holes (Eq. (14)) and thus inhibits the generation of OH^\bullet radical and thereby decreases the degradation rate.

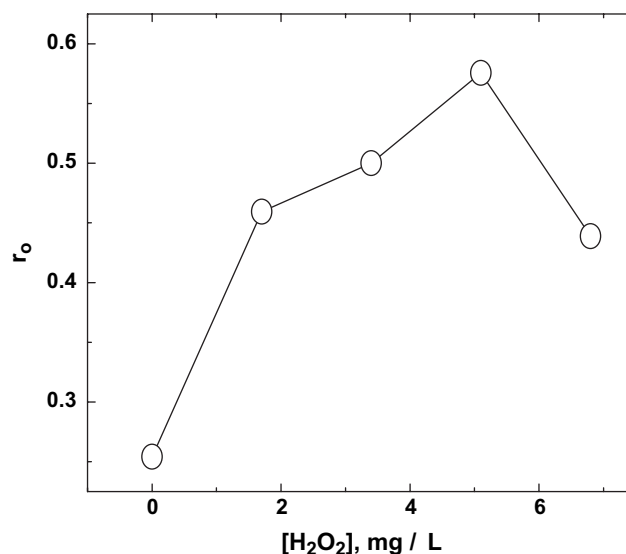
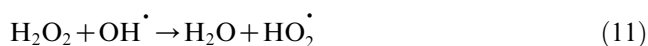


Fig. 8. Effect of H_2O_2 on MB degradation. Conditions: $[\text{MB}] = 10 \text{ mg/L}$; $[\text{Ti–Ag–US}] = 0.25 \text{ mg/L}$; $\text{pH} = 10.0$.



Several researchers have reported the beneficial effect of H_2O_2 on the photocatalytic degradation of pesticides [46,47], benzene, organo phosphorous derivatives, organo halides and dioxins [48,49], whereas a negative effect has also been reported by Chemsidine and Bohem [50] for the degradation of chloro acid on TiO_2 .

3.7. Effect of inorganic salts

The effect of inorganic salts on the degradation process was investigated with common inorganic salts such as nitrate, sulphate and acetate (0.025 M). As can be seen from the Fig. 9, the effectiveness of Ti–Ag–US system was significantly increased in presence of anion. The order of reactivity towards the decomposition of MB was found to be acetate > nitrate > sulphate. Adsorption of MB on TiO_2 was significantly increased in presence of anion species. It can be explained as the reaction of the positive hole (h^+) formed on the Ti–Ag–US with anions and those anions behave like h^+ scavengers resulting prolonged color removal in 0–30 min irradiation. Probably, the adsorbed anions compete with the dye for the photooxidizing species on

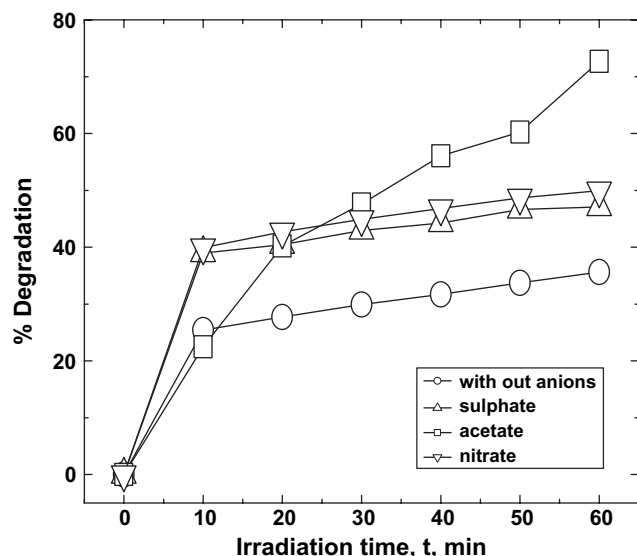


Fig. 9. Effect of common inorganic salts on MB degradation. Conditions: [MB] = 10 mg/L; [inorganic salt] = 250 mg/L; [Ti–Ag–US] = 0.250 mg/L; pH = 6.80.

the surface to form oxidizing inorganic radicals. It is expected that the recombination of h^+ and the electron will be prohibited by these anions leaving the electron for the photodecomposition of MB. It is also expected that some of these radical anions react with the chromophoric groups of surface adsorbed dye and may enhance the rate of degradation. The observed effect is still thought to be strong adsorption of anions on Ti–Ag–US surface [51,52].

3.8. Calculation of relative photonic efficiency

In order to compare the degradation and efficiency of Ti–Ag–US, the relative photonic efficiency (ξ_r) was calculated using Eq. (14).

$$\xi_r = \frac{\text{Rate of disappearance of dye}}{\text{Rate of disappearance of phenol}} \quad (14)$$

where both (initial) the rates are obtained under exactly the same condition. The relative photonic efficiency of the dye degradation is 4.05. The efficiency is greater than unity, indicating that the initial photocatalysed oxidative degradation of the dye is more efficient than for phenol [53].

4. Conclusions

- Nanocrystalline, pure anatase titania doped with silver (Ti–Ag–US) was prepared by sol–gel process via ultrasonic irradiation.

- The average crystallite size calculated from Debye–Sherrer equation was found to be 44 nm.
- It was observed that Ti–Ag–US is efficient for the degradation of MB from aqueous solution.
- From the experimental results, the dependence of the Ti–Ag–US concentration on the initial decolorization rate follows a relationship, $r_0 \propto [\text{TiO}_2]^n$. The value of n was found to be 2.05.
- The photocatalytic rate of MB increased in presence of H_2O_2 .
- The influence of H_2O_2 on the decomposition rate reveals the fact that the most possible oxidation mechanism of MB is the dual hole–radical mechanism.
- The optimum concentration of 5 mg/L of H_2O_2 is required for the effective degradation of 10 mg/L of MB at pH 10.
- The experimental data suggest that the degradation of MB follows pseudo first order kinetics.
- The sol–gel coupled with ultrasonic technique is fast and gives uniform distribution of crystallites of pure anatase titania confirmed by XRD studies.
- Ultrasonication does not only reduce the crystallite size but also enhances the hydrolysis of titanium alkoxide for faster and better crystallization of anatase nano particles.
- From the result of present work and the literature, one could understand that photocatalytic treatment of textile industry waste-water is a promising tool for the decolorization of colored wastewaters.

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